Statement of Basis - Narrative
For an NSR Permit

Company: New Mexico Copper Corporation
Facility: Copper Flat Mine
Permit No(s).: 0365M3
Tempo/IDEA ID No.: 1535 - PRN20130001
Permit Writer: Sam Speaker

Fee Tracking

Tracking	**NSR tracking entries completed:** [] Yes [] No
	NSR tracking page attached to front cover of permit folder: [] Yes [] No
	Paid Invoice Attached: [] Yes [] No
	Balance Due Invoice Attached: [] Yes [] No
	Invoice Comments:

Permit Review	**Date to Enforcement:** TBD	**Inspector Reviewing:** Robert Samaniego
	Date Enf. Review Completed:	**Date of Reply:** (if necessary)
	Date to Applicant: TBD	**Date of Reply:**
	Date of Comments from EPA: TBD or N/A	**Date to EPA:** TBD or N/A
	Date to Supervisor: TBD	

1.0 Plant Process Description:

New Mexico Copper Corporation (NMCC), a wholly owned subsidiary of THEMAC Resources Group Ltd. (THEMAC), is applying to the New Mexico Environmental Department–Air Quality Bureau (NMED AQB) for a 20.2.72.200.A.1 NMAC minor source air quality construction permit for a proposed open pit copper mine identified as “Copper Flat Mine”.

Location

The Copper Flat Project is a copper/molybdenum porphyry deposit located in the Hillsboro Mining District in Sierra County, South Central New Mexico. The center of the mineralization is at approximately UTM coordinates 263,150 meters easting, 3,650,750 meters northing, Zone 13, NAD 83. The Project is approximately 150 miles south of Albuquerque, New Mexico and approximately 20 miles southwest of Truth or Consequences, New Mexico (straight line distances). Access from Truth or Consequences is by 24 miles of paved highway and 3 miles of all-weather gravel road.

History

Development of the Copper Flat Project began in the 1970's by Quintana Mineral Corporation. Quintana Mineral Corporation applied for and received Air Quality Permit #0365. In 1982 operating under Air Quality Permit #0365-M1, the Copper Flat Partnership, Ltd. developed and operated the Project, which consisted of an open pit copper mine, a 15,000-ton per day flotation mill, and a 515-acre Tailings Storage Facility (TSF). The Copper Flat Mine officially commenced full commercial production in April, 1982. In July 1982 the mine was shut down due to low copper prices and other economic considerations. In 1986 all on-site surface facilities were removed and a BLM approved program of non-destructive reclamation was carried out. Most of the property's infrastructure, including building foundations, power lines and water pipelines were preserved for reuse in the future in the event copper prices recovered sufficiently to make re-establishing the Project economically viable. In April of 1995, Alta Gold Company applied for a revision to Air Quality Permit #0365-M1. However, Alta Gold Company declared bankruptcy in early 1999. Air quality permit #0365-M1 was closed in 2002 due to inactivity.

Overview

NMCC is proposing to reopen the Copper Flat Project open pit mine to operate 24 hours per day, seven days per week, and 365 days per year. The mining of new ore would entail expansion of the existing open pit. A portion of the ore body at the Copper Flat Mine is exposed at the surface and would be mined by conventional truck and shovel open pit methods in a manner similar to the previous operation. An operational life of the mine is projected to be approximately 11 years. Over the life of the Project, approximately 159 million tons of material would be mined. The operation would mine an estimated annual average of 15.3 million tons of material per year over years one through 10. Approximately 1.7 million tons would be mined in pre-production and 4.7 million tons in year 11. The crushing operation would process an average 9.1 million tons of ore per year from years one through ten and between 4.0 million and 7.0 million tons in year 11 depending when the low grade ore is milled. Waste rock production is estimated to average 5.7 million tons per year or 60.7 million tons over the life of the mine. Approximately 3.0 million tons total of low grade ore would be mined in years one through three, with the majority of that, 2.5 million tons, being mined in year two. The low grade copper ore would likely be processed during operations as blend material and/or at the end of the mine life, depending on economic conditions at the time. As such, it would require stockpiling until such time at it is suitable for processing.

Mining

Preproduction stripping of overburden was completed in 1982 during the previous operation. Approximately 3 million tons of overburden material was stripped and over 1.2 million tons of ore were mined from the existing pit during the early 1980s. The Copper Flat Mine ore body would be mined by a multiple bench, open pit method. The existing pit would eventually be enlarged to approximately 2,800 feet by 2,800 feet with an ultimate depth of approximately 900 feet. The working, inter-bench slope of the pit walls would range from 38 to 45 degrees, but would be optimized based on on-going evaluations of project economics and pit slope engineering. Ore material from the pit would be drilled and blasted, loaded and hauled out of the pit to the primary crusher. Drilling and blasting will break up the rock in the open pit. Blasting would be limited to daylight (afternoon) hours and performed by licensed blasters. Ammonium nitrate and diesel fuel (ANFO) will be used as the explosive. The broken rock would be loaded onto end dump haul trucks for transport to the primary crusher, low grade stockpile, or waste rock disposal facility (WRDF) depending on the assay classification. Loading of both ore and waste rock would be accomplished by using hydraulic shovels and/or frontend loaders. Ore and waste rock haulage would be handled by a fleet of end-dump, diesel-powered haulage trucks of a 100 ton capacity.

Waste Rock Stockpile

Waste rock disposal facilities (WRDFs) would be located 3,000 to 4,000 feet east of the pit exit. This disposal area would be expanded under the current mine plane of operations (MPO) to cover approximately 180 acres. Total material contained in the disposal areas at the end of the expected life of the project would be approximately 60.7 million tons.

Low Grade Stockpile

The low grade stockpile would cover an area of approximately 20 acres. The total storage planned for the low grade stockpile is 2.87 million tons of low grade ore of rock assaying less than 0.20 percent copper. The low grade stockpile is located to the northeast of the mine. The location was selected to be a reasonable haul during the mine life for the storage of the material, as well as a short haul distance to the crusher at the end of the mine life.

Ore Processing

The primary crusher is to be located about 2,500 feet east of the pit. Run-of –mine (ROM) ore is trucked from the mine to the primary crusher where it is dumped directly into the crusher surge bin that feeds a gyratory crusher, which crushes the ROM ore to a nominal size of less than eight inches in diameter. Delivery of ore by truck would be on a schedule similar to the mining operations. The crusher is located below ground level to limit noise and contain dust. Crusher discharge would be fed by apron feeder onto a belt conveyor for transport to the coarse ore stockpile located near the mill. Water sprays are used during loading of the surge bin to control fugitive dust. Dust emissions during primary crushing and transfer points within the crusher vault will be controlled with dust collection equipment (i.e., bag houses).

Storage capacity of the coarse ore stockpile would be about 75,000 tons. Fugitive dust during loading of the stockpile would be controlled with water sprays at the point where the stockpile feed conveyor dumps to the stockpile. During primary crusher down time, ore at the coarse ore stockpile would be moved from the "dead" storage area to the "live" storage area by front-end loader or bulldozer.

Two reclaim chutes beneath the coarse ore stockpile would direct ore onto apron feeders and feed ore onto a belt conveyor for transport into a large diameter semi-autogenous (SAG) mill for the first stage of grinding. Dust emissions from the reclaim operations will be controlled with dust collection equipment (i.e., bag houses).

Reduction in the SAG mill would be a result of impact between the ore chunks, and between the ore chunks and the five inch steel grinding balls used in the mill. Reduction would be a combination of crushing and attrition. Water and various chemicals/reagents would be added to the SAG mill feed to start the conditioning of the ore pulp for subsequent stages of treatment. Tonnage of the primary feed to the SAG mill would be a nominal 25,000 tons per day. The SAG mill would discharge onto a vibrating screen. Undersize crushed ore from the screen would report to a cyclone feed sump. The oversize ore would be taken by belt conveyor to a pebble crusher, where it would be crushed to less than 0.75 inch in diameter and returned by belt conveyor to the SAG mill. Oversize ore from the SAG mill discharge may also be diverted around the pebble crusher and returned by conveyor to the SAG mill or stockpiled. Ore from the cyclone feed sump would be pumped to a cluster of hydro-cyclones for material sizing. The fines would report to the first stage of flotation, and the oversize ore would report to the ball mill for further grinding. The ball mill discharges to a cyclone feed sump. The contents of the sump are transferred by pump to a hydrocyclone cluster. A bleed from the hydrocyclone underflow feeds a Knelson gravity concentrator to remove gravity recoverable gold before returning to the circuit. The hydrocyclone underflow reports back to the ball mill and the overflow reports to the flotation plant.

The flotation plant will consist of copper and molybdenum flotation circuits. The copper and molybdenum minerals will be concentrated in a bulk copper/moly concentrate. The moly mineral will be separated from the copper minerals in a moly flotation circuit. The bulk (copper-moly) flotation circuit will consist of rougher flotation, concentrate regrind, first cleaner /first cleaner/scavenger flotation, and second cleaner flotation. The moly flotation circuit will consist of moly separation (rougher) flotation, moly first cleaner flotation, concentrate regrind, moly second cleaner flotation and moly third cleaner flotation.

Final copper concentrate will be thickened, filtered, and loaded in trucks for shipment.

Final molybdenite concentrate will be thickened, filtered, dried, and packaged into containers for shipment. Drying of the molybdenum concentrate will be done with a Holoflite type electrically heated (line power) oil that dries the molybdenum concentrate as it travels through an enclosed screw conveyor.

From the SAG mill loading to the final concentrate all processes are wet, with no expectation of particulate emissions. Fugitive emissions generated during loading of the copper concentrate into trucks will be controlled by performing all operations in the enclosed mill building. Fugitive emissions generated during drying and loading of the molybdenum concentrate into sacks/trucks will be controlled with a dust collection system (i.e., bag houses).

Tailings

An existing tailings storage facility (TSF) at Copper Flat was constructed by Quintana Minerals to serve their 1982 mining operation. The facility received 1.2 million tons of material and was essentially reclaimed in 1986. The tailings impoundment remains in place and is located southeast of the former plant site. NMCC proposes to construct a new lined (TSF) over the area used by previous operations for tailings disposal. Tailings would be transported from the mill via slurry pipeline and deposited in the new facility. Approximately 100 million tons of tailings are expected to be impounded over the life of the project.

Tailings from the bulk rougher flotation process are transported to the TSF where hydrocyclones are used to produce sands to build the centerline TSF dam. The cyclone overflow is deposited to the interior of the impoundment and produces a supernatant water pond. The water pond is used to reclaim water from the tailings for reuse in the milling process.

During TSF dam construction, bulldozers and compactors will be used to compact the sands used to construct the dam.

During the initial 4 years of operating the mine and mill, topsoil will be removed from the tailing area and stored in borrow storage piles adjacent to the tailing area. This activity will be performed with scrapers. It includes scraper loading of topsoil, scraper unloading of topsoil onto the piles, and scraper travel. Fugitive dust will be controlled by watering during scraper travel.

Haul Roads and On-Site Service Roads

For the most part, existing haul roads will be utilized to haul material to the crusher, stockpiles, and WRDF. Some minor realignment of these roads may be necessary and road widths would vary. Haul roads are not expected to create new disturbances, as they would be constructed on previously disturbed land. The on-site roads would be designed for easy access and traffic movement within the operations area. Waste rock and ore would be hauled to the disposal areas and primary crusher using conventional mining haul trucks. During operation of the Copper Flat Project, water trucks would be used, as needed, to control emissions of fugitive dust from the haul roads, and other roads within the project area. Wetting agents and binding agents, such as magnesium chloride, may also be used to control dust if conditions warrant.

Chemicals/Reagents

Chemicals/Reagents used as part of the copper/molybdenum concentrating process would include frothers, flotation promoters, flotation collectors, flocculants, flotation reagents, and pH regulators. These chemicals/reagents would be delivered by truck from commercial sources to the mine site where facilities would be provided for off-loading, storing, mixing, handling, and feeding. Chemicals/reagents that are received dry would be mixed in agitation tanks and pumped to either outdoor storage tanks or liquid storage tanks inside the concentrator building from which they would be metered into the concentrating process. Residual chemical/reagent concentrations in the tailings and reclaim water streams are expected to be present at very low levels since they would be added to water in amounts resulting in concentrations of approximately 3 parts per million (ppm). Also, normally 95 percent of the chemicals/reagents would be adsorbed onto the copper or molybdenum mineral surface and floated off in the mineral froth. The chemicals/reagents would then be subsequently consumed in the offsite smelting process. Assuming 95 percent of the chemicals/reagents are adsorbed, the residual chemicals/reagents reporting to the tailings stream drops to less than 0.15 ppm.

Frother reagents to be used at the mine include methyl isobutyl carbinol (MIBC). MIBC is biodegradable in low concentrations. The dosage rate would be 0.12 pound per ton of mill feed. The bulk of this reagent would report to the concentrate fraction and end up at the smelter. The reagent would be received in trucks and stored in a tank inside the concentrator building.

Lime used in alkalinity control in the flotation circuit would be received in bulk pebble form by 20 ton capacity trucks and stored in a 500 ton capacity storage silo. The lime would then be slaked with water in a small mill and the resulting “milk of lime” would be pumped to the addition points in the grinding and flotation circuits for use as a pH regulator. It is anticipated that lime would be used at a rate of 2.4 pounds per ton of mill feed to control pH of the flotation circuit. During the milling process, most of the lime would react with sulfide minerals to form gypsum. The lime storage silo and associated milk of lime tanks are located outside and adjacent to the concentrator building on a concrete slab designed to accommodate secondary containment of the liquid constituents.

Ammonium Nitrate Prill is the dry component of ANFO. It will be stored in a 50 ton capacity storage silo southeast of the open pit. Annual throughput of prill will be 3,650 tons per year. Ammonium nitrate prill comes in the form of pellets. The physical properties of prill (low silt content) are conducive to minimal fugitive dust during silo loading.

Sodium hydrosulfide (NaSH) would be added to the circuit process as a moly depressant to affect the copper molybdenum separation. These chemicals/reagents are rapidly oxidized through contact with copper minerals and air bubbles entrained in flotation pulp. These chemicals/reagents would be transferred from a delivery truck to appropriate on-site mixing and distribution tanks.

Number 2 diesel fuel would be used as a molybdenum collector. This diesel would be stored in a tank inside the concentrator building. Antiscalants such as NALCO9731, NALCO9735 (or equivalent) would be stored in tote containers, which are 250 pound double walled plastic containers that can be moved with a forklift.

Number 1 diesel fuel for mobile equipment would be stored onsite on a self-contained fuel and lube skid, including two 20,000-gallon, double-walled tanks with multiple lube and coolant capacity. This skid-mounted assembly would be staged near the truck ready line. Diesel fuel tanks onsite would be installed in conformance with applicable New Mexico Environment Department Petroleum Storage Tank Bureau regulations for New Storage Tank Systems in 20.5.4 NMAC. As required, secondary containment shall be constructed with a capacity of at least 110% of the size of the largest above ground storage tank (AST) in the containment area plus the volume displaced by the other AST(s). The geo-synthetic membrane for secondary containment shall have a minimum thickness of 60 mils.

Chemicals/reagents would be maintained in the Reagent Area of the Concentrator Building, constructed of 8” concrete block walls and a metal roof.

- Reagents such as Xantate (K.Amyl) (or equivalent): This flotation collector reagent would be kept in drums and transferred to a mixing tank, then to a holding tank, and finally to the head tank;
- AEROFLOAT 238 (also known as Butyl Dithiophospate or equivalent): used in flotation promoting, would be kept in drums and transferred to a mixing tank, then to a 6-ft diameter, 8-ft high holding tank, and finally to a 6-ft diameter, 8-ft high head tank.
- MIBC (or equivalent): MIBC would be transferred from trucks to a holding tank, and, as needed, to a head tank.
- Use of small amounts (<100 pounds) of sulfuric acid would be limited to the laboratory.
- Number 2 Diesel Fuel: For use in the copper-moly flotation process will be stored in a tank.
- Sodium Hydrosulfide: For use in the copper-moly circuit as a depressant to facilitate the separation of moly from copper are stored in a mixing and distribution tanks.

Potential reagent spills would be contained by curbs in the reagent mixing and storage areas. A floor sump pump would be used to return the spilled material either to the storage tank or into the milling process as necessary.

Estimated reagent consumption rates are presented as Table 3-1.

Table 3-1: Estimated Reagent Consumption Rates for Sulfide Ore

Item	**Rate lbs/ton ore**
Copper Circuit	
Collector, Potassium Amyl Xanthate	0.030
Collector, Butyl Dithiophosphate	0.010
Frother, Methyl Isobutyl Carbinol (MIBC)	0.12
Collector, #2 Diesel Fuel	0.1
Lime (90% CaO)	2.4
Flocculant (for Concentrate Dewatering)	0.01
Molybdenite Circuit	
Sodium Hydrosulfide	0.25
#2 Diesel Fuel	0.007
Methyl Isobutyl Carbinol (MIBC)	0.007

Air Quality Issues

The Copper Flat Project would be designed to control particulate emissions to meet all regulatory standards. As per New Mexico state regulation 20.2.72 NMAC, the project air quality construction permit must be authorized by the New Mexico Environment Department prior to project commencing.

Emission rate calculations were based on an operating scenario that determines potential emissions representing a worst-case scenario from the facility. The emissions from mining and milling are based on an annual processing rate of 9,125,000 tons of ore. This is the expected amount of ore that will be processed through the mill. In addition to the ore processed through the crusher and mill the facility will also handle low grade ore and waste rock handled from the pit. The amount of material delivered to the low grade ore and waste rock storage areas is based on the expected annual average amount of material handled over the life of the mine. Truck traffic estimated emissions are based on moving the material at the throughputs discussed above. Bulldozer hours of operation pushing material in the pit, at the low grade ore and waste rock stock piles, and the tailing area are based on typical mining practices at similar facilities.

Committed air quality practices would include dust control for mine unit operations. In general, the fugitive dust control program would provide for water application on haul roads and other disturbed areas; chemical dust suppressant application (such as magnesium chloride) where appropriate; and other dust control measures as per accepted and reasonable industry practice. Also, disturbed soils would be seeded with an interim seed mix to minimize fugitive dust emissions from un-vegetated surfaces where appropriate. Fugitive emissions in the process area would be controlled at the crusher, stockpile reclaimer, and conveyor drop points through the use of fugitive dust collectors. Other process areas requiring dust and/or emission controls include the concentrate drying and packaging circuit and the various process plants. Appropriate emission control equipment would be installed and operated in accordance with the air quality construction permit. The lime storage would be fitted with a dust collector for capture of fugitive dust during loading of the lime silo.

Deposition of tailings would be done by spigotting and/or cyclone discharge. By this procedure, the surface would be wet, thereby eliminating or reducing fugitive dust. As necessary, control of fugitive dust in the vicinity of the TSF would be attained by watering. After reclamation, the TSF would be covered with growth medium and vegetated.

No gaseous contaminants, with the exception of blasting, are expected to be emitted to the atmosphere from the proposed stationary source operations. Drilling operations would be done wet or with other efficient dust control measures. At a minimum, haul roads, waste rock disposal areas, and ore transfer points would be wetted down on a regular basis to minimize dust emissions. Fugitive SO_2 emissions from ore and the flotation equipment are expected to be small due to the low volatility of the sulfur compounds present in the concentrate.

2.0 Description of this Modification:

Though this facilities permit number would imply that this is a modification. This permit is starting from scratch. There is no current operation to modify.

3.0 Source Determination:

1. The emission sources evaluated include those listed in Table 2-A of the application.

2. Single Source Analysis:
   A. SIC Code: Do the facilities belong to the same industrial grouping (i.e., same two-digit SIC code grouping, or support activity)? Yes all the equipment listed in Table 2A of the application belong to the same SIC code.
   B. Common Ownership or Control: Are the facilities under common ownership or control? Yes, all the equipment listed in Table 2A of the application is under common control.
   C. Contiguous or Adjacent: Are the facilities located on one or more contiguous or adjacent properties? Yes, all of the equipment listed in Table 2A of the application is on the same or contiguous property.

3. Is the source, as described in the application, the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes? Yes

4.0 PSD Applicability:

A. The source, as determined in 3.0 above, is a minor source before and after this modification.

5.0 History (In descending chronological order, showing NSR and TV):

*The asterisk denotes the current active NSR and Title V permits that have not been superseded.

Permit Number	Issue Date	Action Type	Description of Action (Changes)
0365M3	TBD	New	Please see above
0365M2			This facility has been dismantled and no longer exists.
0365M1			This facility has been dismantled and no longer exists.
0365			This facility has been dismantled and no longer exists.

6.0 Public Response/Concerns:

As of April 8, 2013 this permit writer is aware of two public comment or concern.

7.0 Compliance Testing:

Unit No.	Compliance Test	Test Dates
	No conditions requiring initial compliance testing is planned to include at this time.	

8.0 Startup and Shutdown:

A. If applicable, did the applicant indicate that a startup, shutdown, and emergency operational plan was developed in accordance with 20.2.70.300.D(5)(g) NMAC?
B. If applicable, did the applicant indicate that a malfunction, startup, or shutdown operational plan was developed in accordance with 20.2.72.203.A.5 NMAC?
C. Did the applicant indicate that a startup, shutdown, and scheduled maintenance plan was developed and implemented in accordance with 20.2.7.14.A and B NMAC?
D. Were emissions from startup, shutdown, and scheduled maintenance operations calculated and included in the emission tables?

9.0 Compliance and Enforcement Status [Title V only]:

Not a Title V source

10.0 Modeling:

Modeling is being reviewed by Mr. Eric Peters of the New Mexico Environment Department,

11.0 State Regulatory Analysis(NMAC/AQCR):

20 NMAC	Title	Applies (Y/N)	Comments
2.1	GENERAL PROVISIONS	Yes	The facility is subject to Title 20 Environmental Protection Chapter 2 Air Quality of the New Mexico Administrative Code so is subject to Part 1 General Provisions, Update to Section 116 of regulation for Significant figures & rounding. Applicable with no permitting requirements.
2.3	Ambient Air Quality Standards	Yes	20.2.3 NMAC is a SIP approved regulation that limits the maximum allowable concentration of Total Suspended Particulates, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide.
2.7	Excess Emissions	Yes	Applies to all facilities' sources
2.61	Smoke and Visible Emissions	Yes	The Engines EG1 and EG2 are Stationary Combustion Equipment.

20 NMAC	Title	Applies (Y/N)	Comments
2.70	Operating Permits	No	Title V does not include fugitive emissions toward applicability unless they are a listed source or are subject to an New Source Performance Standards Proposed or National Emission Standards For Hazardous Air Pollutants promulgated prior to August 7, 1980. This facility is not a listed source not is it subject to a NSPS or a MACT published before August 7, 1980. The Title V applicability threshold is 100 tpy. The facility requested allowable is 657 tpy for TSP. If we start to subtract the units that are easily identified as fugitives, we are less than 100 tpy of TSP from point (non fugitive) sources. Therefore, this facility is a Title V minor source. 657 Requested allowable -19 Unit S1 - Open Pit Drilling -20 Unit S22 - Bull Dozer -30 Unit S24 – Bull Dozer -319 Unit S29 – Bull Dozer -28 Unit S28 – Scraper Travel -44 Unit S4 – Open pit haul trucks -41 Unit S5 - Open Pit Bulldozing -21 Unit S11 – Truck unloading -17 Unit S23 - Truck Unloading -13 Unit S30 - Truck Traffic -14 Unit S33 - Wind Erosion + 91 91 < 100 => Not a Title V Major Source
2.72	Construction Permits	Yes	The PER is greater than 25 tpy.
2.73	NOI & Emissions Inventory Requirements	Yes	The PER is greater than 10 tpy

20 NMAC	Title	Applies (Y/N)	Comments
2.74	Permits-Prevention of Significant Deterioration	No	PSD does not include fugitive emissions toward applicability unless they are a listed source or are subject to an New Source Performance Standards Proposed or National Emission Standards For Hazardous Air Pollutants promulgated prior to August 7, 1980. This facility is not a listed source not is it subject to a NSPS or a MACT published before August 7, 1980. Therefore the PSD applicability threshold is 250 tpy. The facility requested allowable is 657 tpy for TSP. If we start to subtract the units that are easily identified as fugitives, we are less than 250 tpy of TSP from point (non-fugitive) sources. Therefore, this facility is a PSD minor source. 657 Requested allowable -19 Unit S1 - Open Pit Drilling -20 Unit S22 - Bull Dozer -30 Unit S24 – Bull Dozer -319 Unit S29 – Bull Dozer -28 Unit S28 – Scraper Travel -44 Unit S4 – Open pit haul trucks -41 Unit S5 - Open Pit Bulldozing -21 Unit S11 – Truck unloading -17 Unit S23 - Truck Unloading -13 Unit S30 - Truck Traffic -14 Unit S33 - Wind Erosion 91 91<250 => Not a PSD major Source
2.75	Construction Permit Fees	Yes	This facility is subject to 20.2.72 NMAC
2.77	New Source Performance	Yes	Applies to any stationary source constructing or modifying and which is subject to the requirements of 40 CFR Part 60, as amended through January 31, 2009 and 40 CFR 60 Subpart LL and IIII applies.
2.78	Emissions Standards for HAPs	No	This facility is a Minor Source of HAPs
2.79	Permits – Nonattainment Areas	No	This facility is not located in a non-attainment area.

20 NMAC	Title	Applies (Y/N)	Comments
2.82	MACT Standards for Source Categories of HAPs	Yes	This regulation applies to all sources emitting hazardous air pollutants, which are subject to the requirements of 40 CFR Part 63, as amended through January 31, 2009 and 40 CFR 63 Subpart ZZZZ applies. This facility is an area source of HAPs.

12.0 <u>Federal Regulatory Analysis:</u>

Air Programs Subchapter C (40 CFR 50)	National Primary and Secondary Ambient Air Quality Standards	Applies (Y/N)	Comments
C	Federal Ambient Air Quality Standards	Yes	Independent of permit applicability; applies to all sources of emissions for which there is a Federal Ambient Air Quality Standard.

NSPS Subpart (40 CFR 60)	Title	Applies (Y/N)	Comments
A	General Provisions	Yes	Applies if any other subpart applies and LL and IIII applies
40 CFR Part 60 Subpart LL	Standards of Performance for Metallic Mineral Processing Plants	Yes	S7-S10, S12-S14, and S16-S20 RE SUBJECT TO 40 CFR 60, Subpart A and LL.
40 CFR Part 60 Subpart IIII	Standards of Performance for Stationary Compression Ignition Internal Combustion Engines	Yes	The provisions of this subpart are applicable to manufacturers, owners, and operators of stationary compression ignition (CI) internal combustion engines (ICE) as specified in paragraphs (a)(1) through (3) of this section. For the purposes of this subpart, the date that construction commences is the date the engine is ordered by the owner or operator. EG1 Exempt Unit – No information given To be used < 500 hrs/yr and during unavoidable loss of commercial power. EG2 No information given To be used < 500 hrs/yr and during unavoidable loss of commercial power.

NESHAP Subpart (40 CFR 61)	Title	Applies (Y/N)	Comments
A	General Provisions	No	

MACT Subpart (40 CFR 63)	Title	Applies (Y/N)	Comments
A	General Provisions	Yes	Applies if any other subpart applies and ZZZZ applies
40 CFR 63 Subpart ZZZZ	National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (RICE MACT)	Yes	A facility is subject to this subpart if they own or operate a stationary RICE at a area source of HAP emissions. EG1 Exempt Unit – No information given To be used < 500 hrs/yr and during unavoidable loss of commercial power. EG2 No information given To be used < 500 hrs/yr and during unavoidable loss of commercial power.

13.0 **Exempt and/or Insignificant Equipment that do not require monitoring**:

NSR Exempt Equipment (not entered into Tempo database)

Description		JUSTIFICATION
EG1	Emergency Generator	**20.2.72.202.B.3**
EG2	Emergency Generator	**20.2.72.202.B.3**
FTK1	Diesel Fuel	**20.2.72.202.B.2.b**
3014-TK-004	No. 2 Diesel Storage Tank	**20.2.72.202.B.2.b**
Other	Other equipment is listed in Table 2-B of the application, but they are not a source of emissions.	

14.0 **New/Modified/Unique Conditions** (Format: Condition#: Explanation):

This permit has not yet been drafted. Please contact Sam Speaker at (505) 476-4351 if you wish to comment on the draft permit before it is issued.

15.0 **Cross Reference Table between NSR Permit 0365 and TV Permit Not a Title V source.**

N/A, this is not a Title V source.

16.0 Permit specialist's notes to other NSR or Title V permitting staff concerning changes and updates to permit conditions.

A.
B.